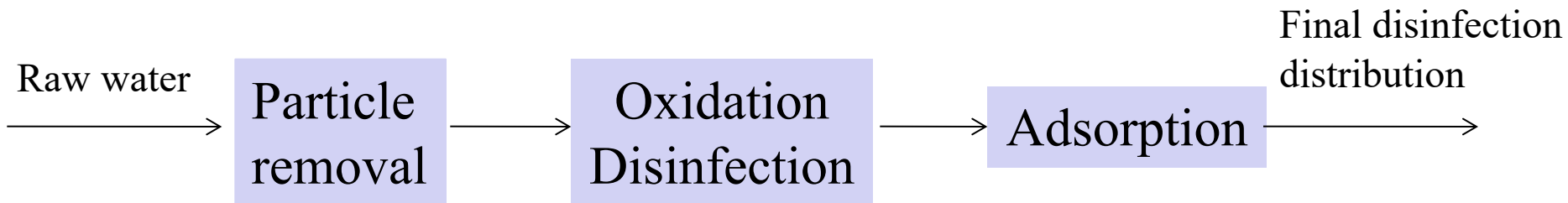


# Adsorption processes

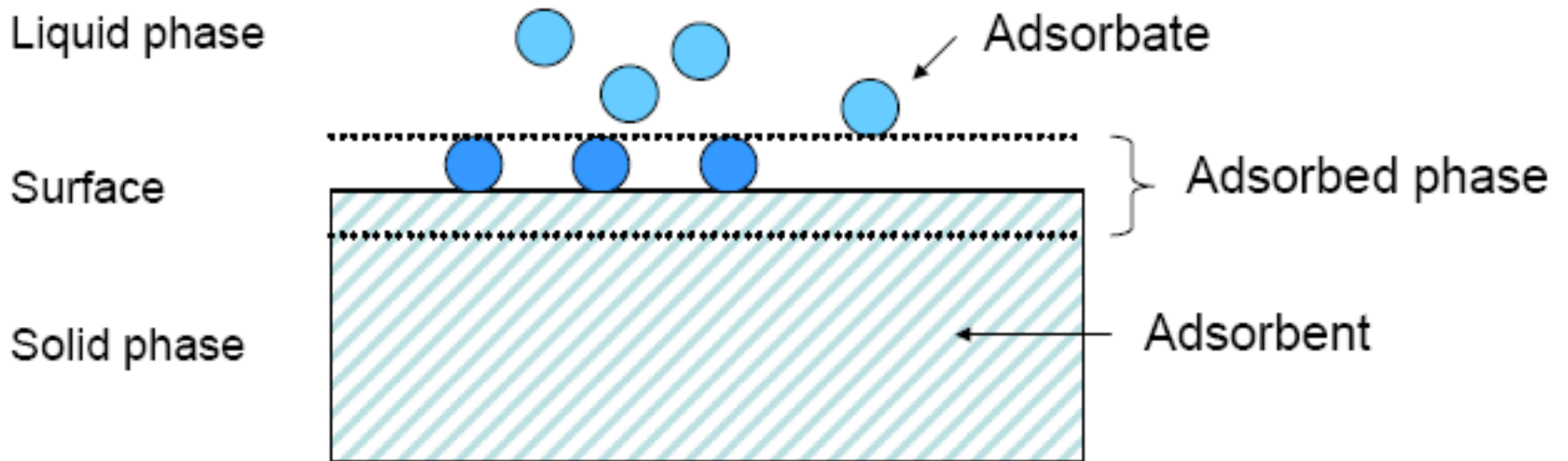
Urs von Gunten

# Role of adsorption processes

- Adsorption processes are widely used in water treatment for micropollutant removal
- Zeolites, synthetic polymeric adsorbents, **activated carbon**
- Typically used in process combinations as a polishing treatment



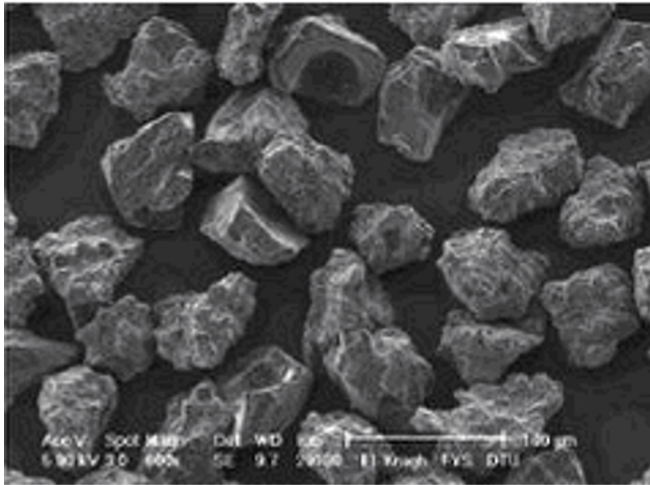
# Adsorption processes



# Activated carbon

## Granular activated carbon (GAC)

Ø 0.5 - 2 mm



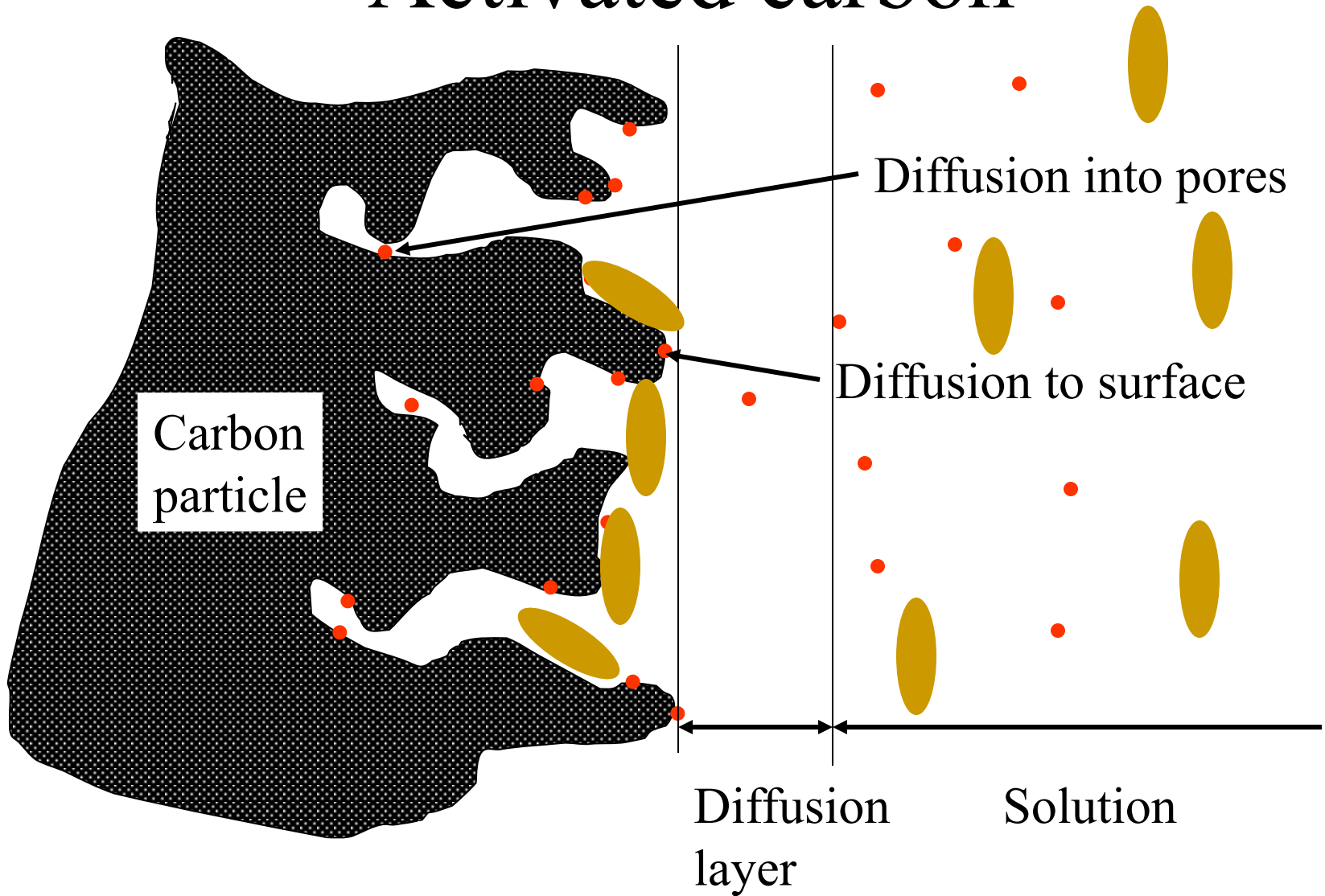
## Powdered activated carbon (PAC)

Ø 0.04 – 0.07 mm



High internal surface areas  
400 - >1500 m<sup>2</sup>/g  
Ca. 10 tennis courts/g  
Adsorption capacity up to  
0.2g adsorbate/g adsorbent

# Activated carbon



-  Natural organic matter (NOM)
-  Molecules

# Activated carbon

- Deep bed, powdered carbon
- Adsorption processes → kinetics, affinity
- Adsorption can be described by empirical equations
- Langmuir isotherm (not shown here)
- Freundlich isotherm for compound S:

$$C_s = K \cdot C_w^{1/n} \rightarrow \log C_s = \log K + 1/n \log C_w$$

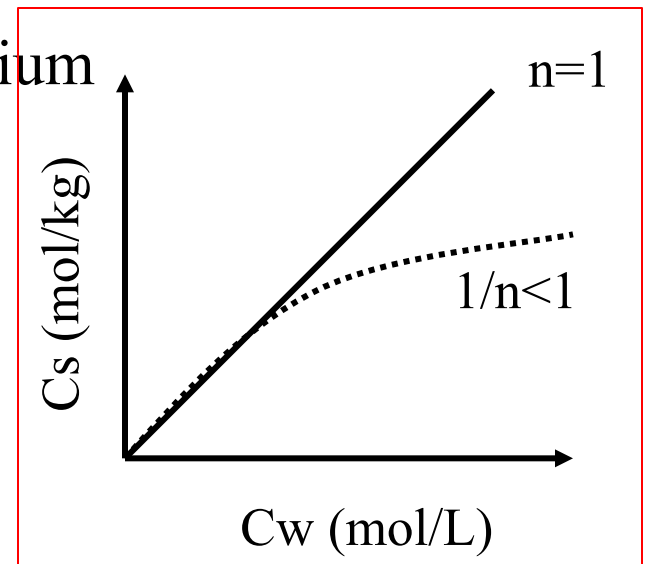
$C_s$  = Amount of S adsorbed per mass unit activated carbon

$C_w$  = Aqueous concentration of S in equilibrium

$K$  = Freundlich constant (mg/g)(L/mg)<sup>1/n</sup>

1/n = Freundlich exponent

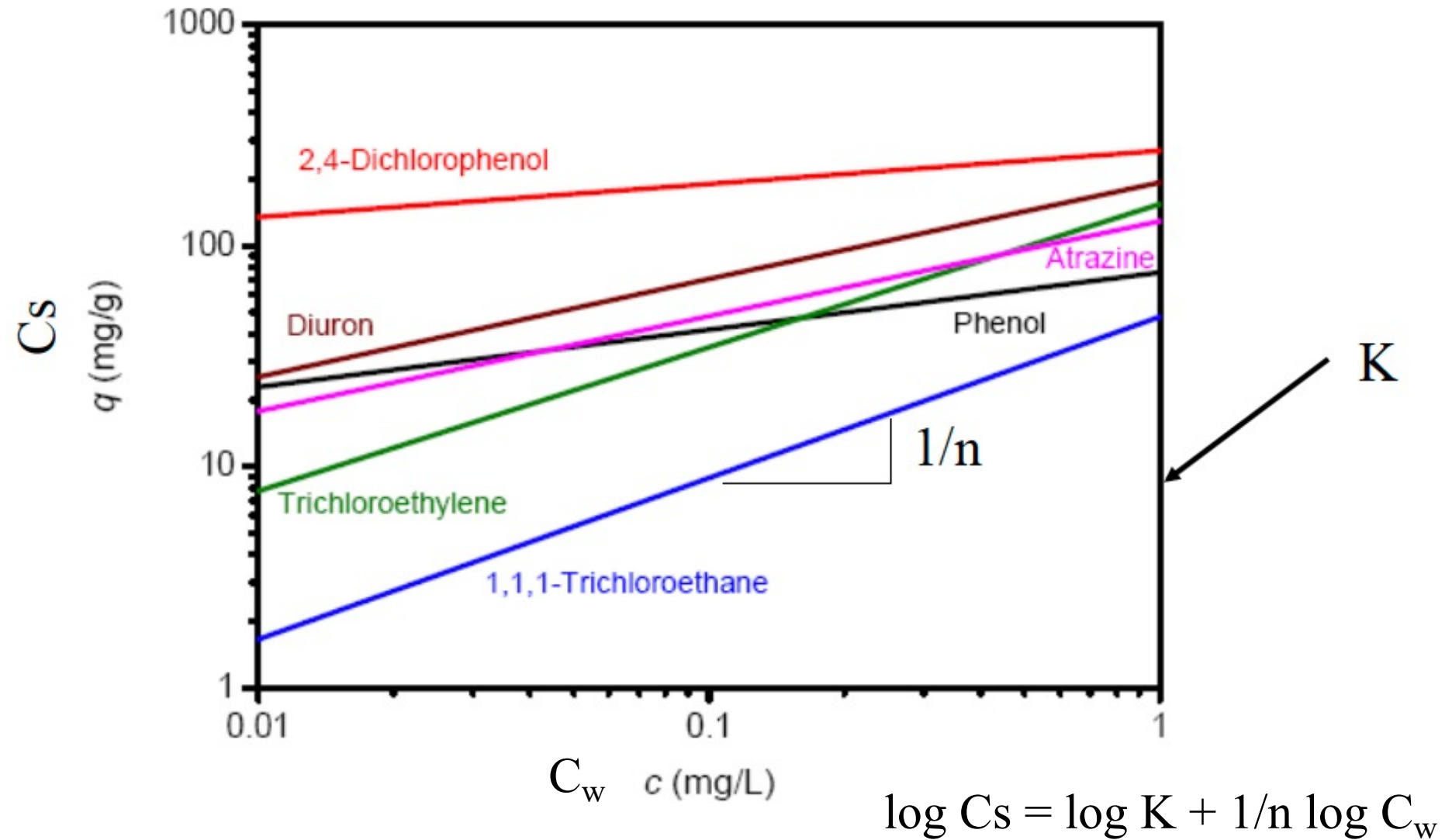
n=1 or  $C_w$  small  $\Rightarrow$   $K = K_d = C_s/C_w$



# Adsorption isotherms: Batch tests

Freundlich log-log plot

AC: F300



# Adsorption on activated carbon

Compound	$\log K_d$ <sup>1)</sup>	$\log K_{ow}$ <sup>2)</sup>
Methyltertbutylether (MTBE)	1.3	0.94
Chloroform	1.6	0.91
Trichlorethen	2.8	2.4
Tetrachlorethen	3.3	2.9
Atrazin	4.1	2.65
Geosmin	3.9	

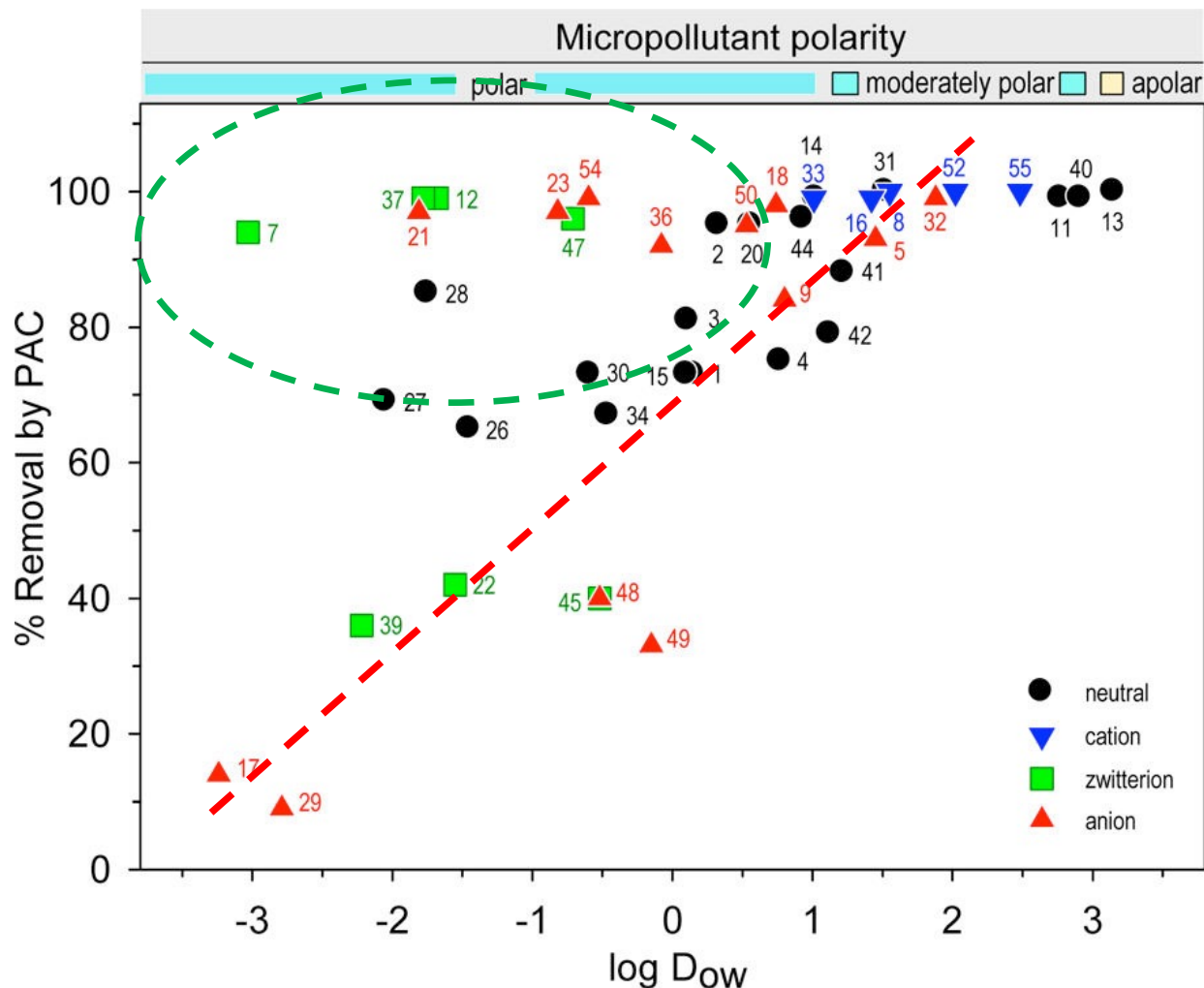
1) Blum et al. 1994, 2) Schwarzenbach et al. 2003

$K_d$ : AC/water distribution coefficient

$K_{OW}$ : Octanol/water distribution coefficient



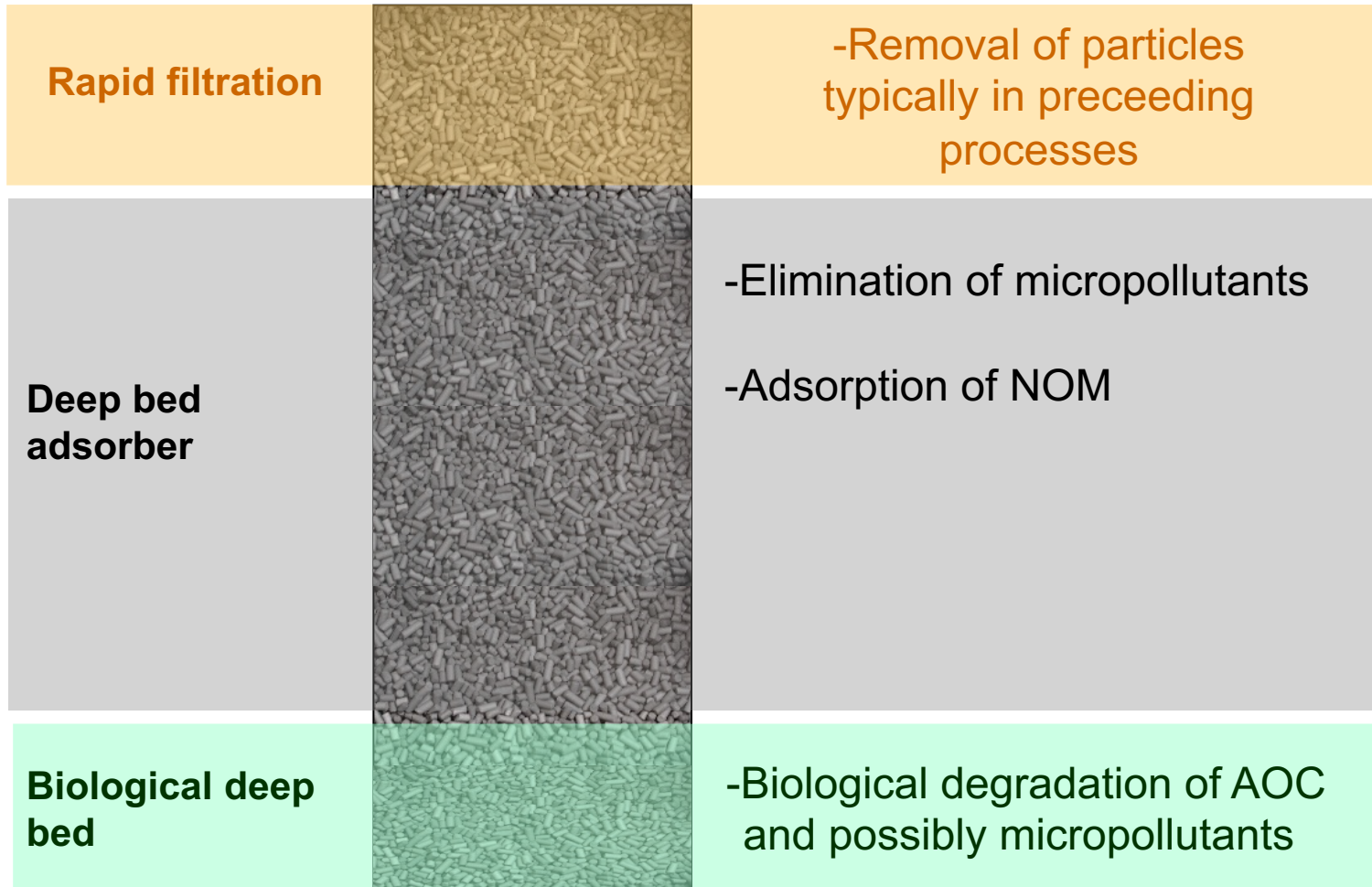
# Removal of micropollutants with PAC from a hospital wastewater



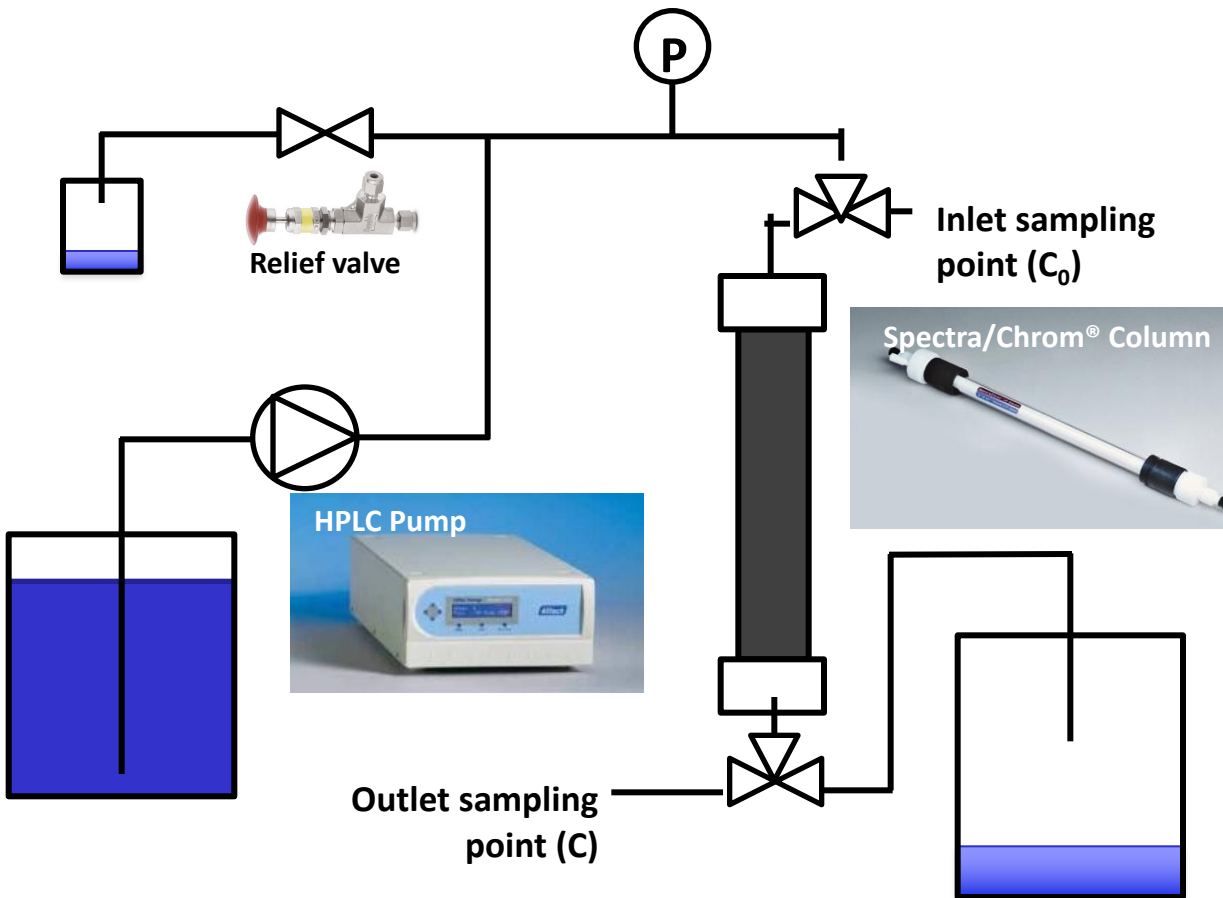
PAC: 23 mg/L  
pH: 8.8  
DOC ca. 7 mg/L

$D_{ow}$ :  $K_{ow}$  corrected for acid-base speciation

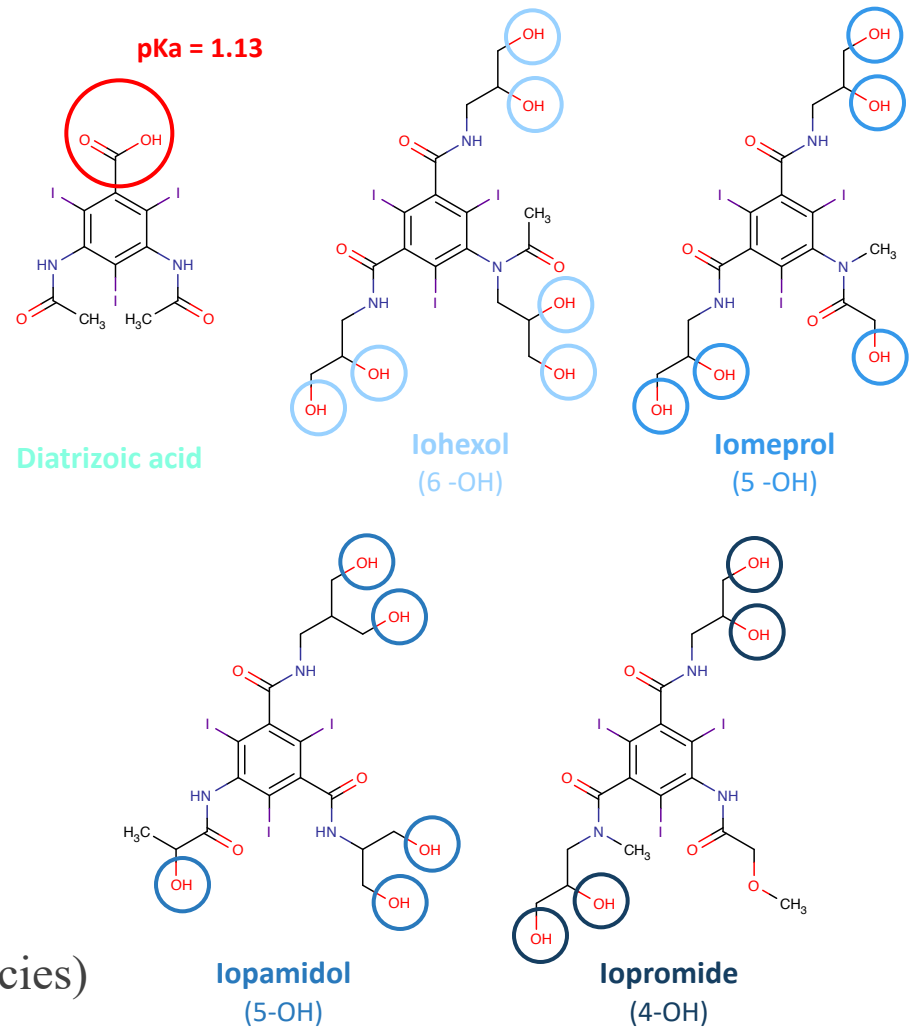
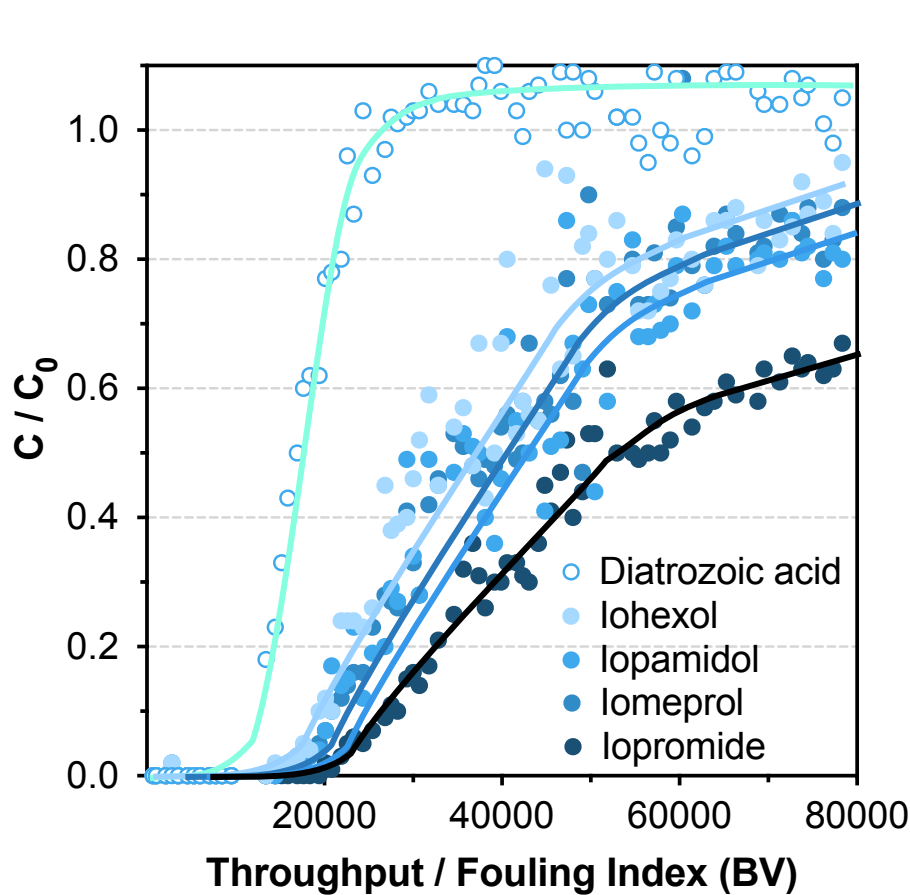
# Purposes of an activated carbon filter



# Rapid small-scale column tests



# Micropollutant breakthrough - X-ray contrast media

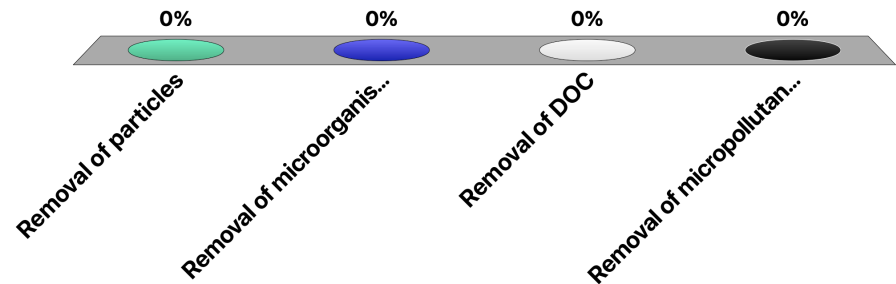


Diatrizoic acid breaks through first (anionic species)

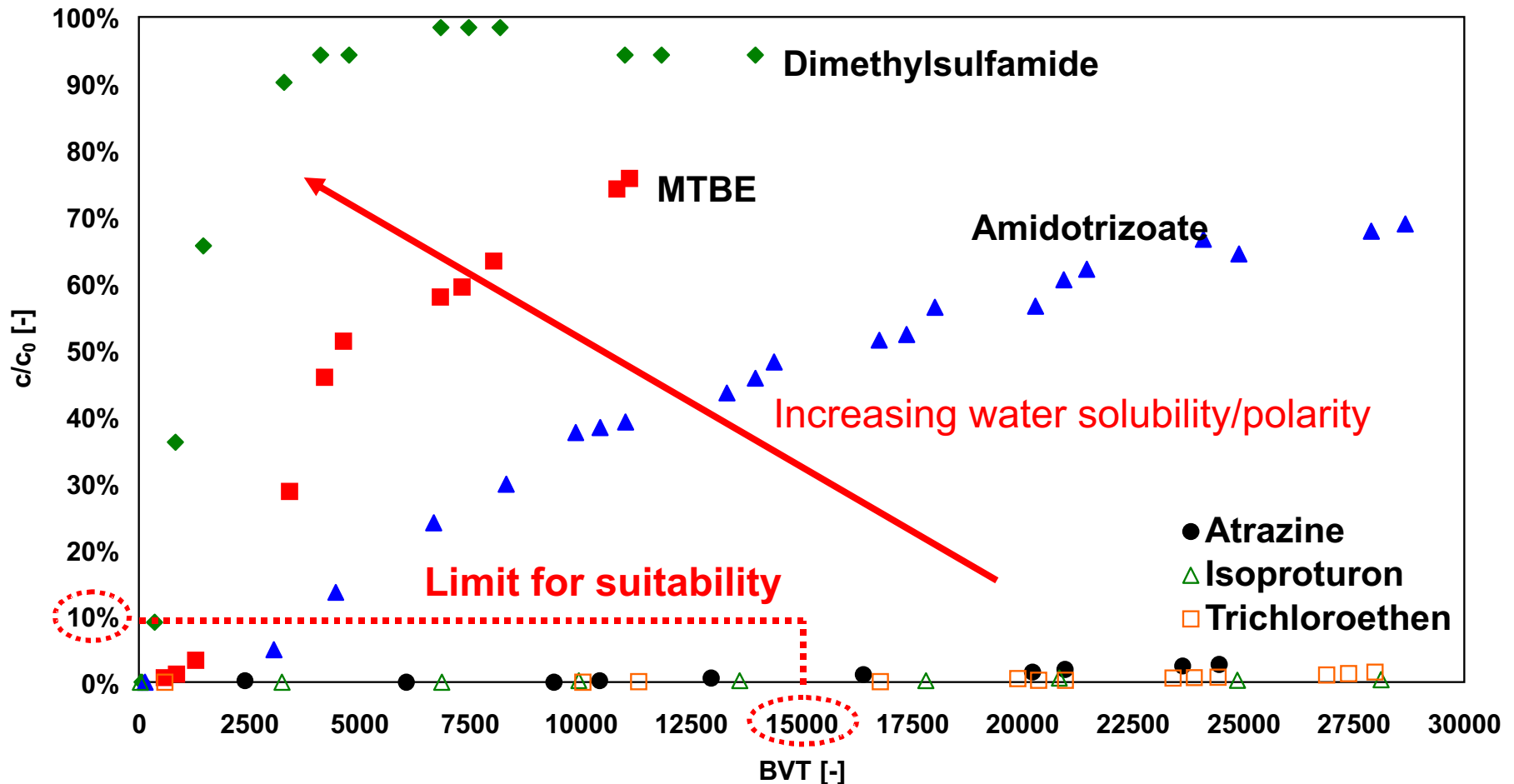
Possible relation between adsorption and the number of hydroxyl groups (-OH).

# The main purpose of the application of activated carbon is..

- A. Removal of particles
- B. Removal of microorganisms
- C. Removal of DOC
- D. Removal of micropollutants



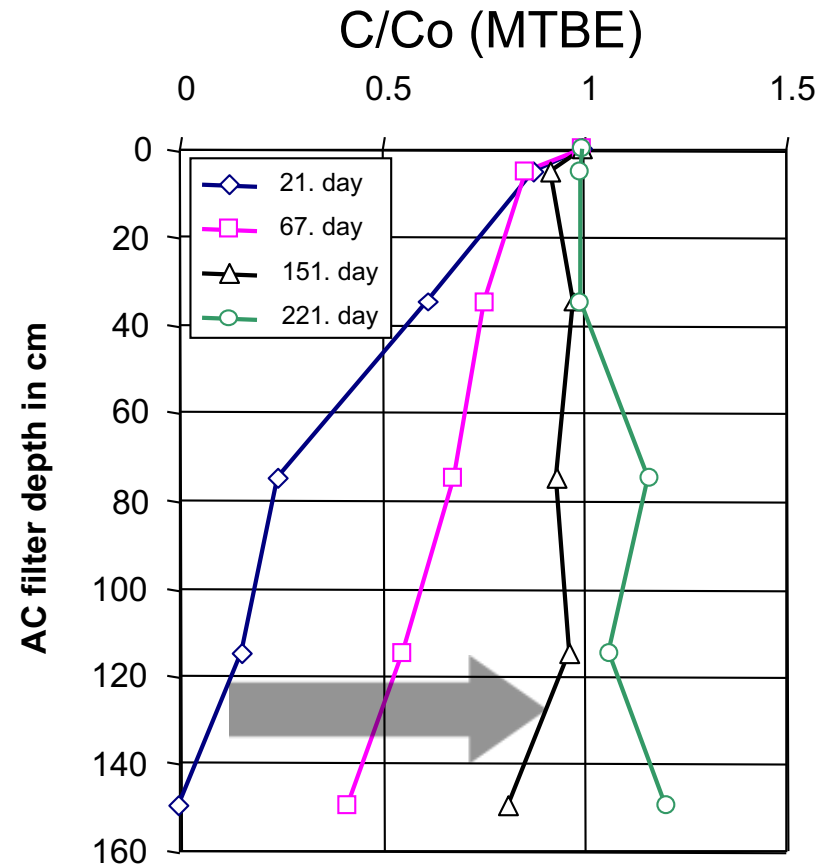
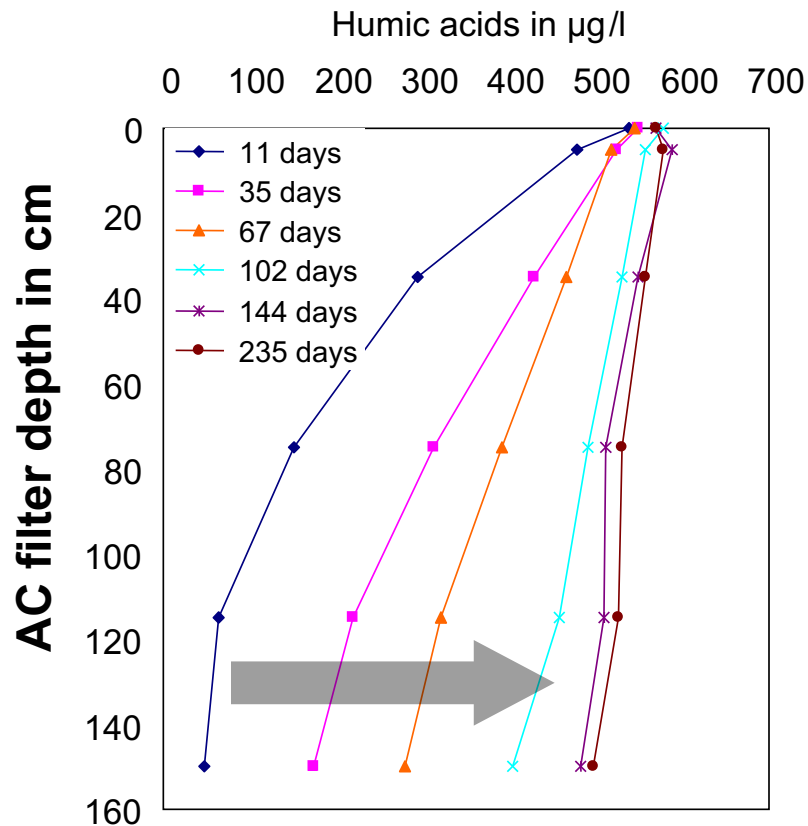
# Standard Laboratory tests with small-scale activated carbon filters: Breakthrough of selected compounds



8 mL/min, diameter of filter 10 mm, amount carbon F300: 1.6g, average grain diameter 385  $\mu\text{m}$ , EBCT  $\approx$  25 s, inlet concentration 25  $\mu\text{g/L}$ , tap water Karlsruhe

# Behaviour of humic acids and MTBE in a pilot plant activated carbon filter (Lengg, Zürich)

## Humic acids Part of NOM



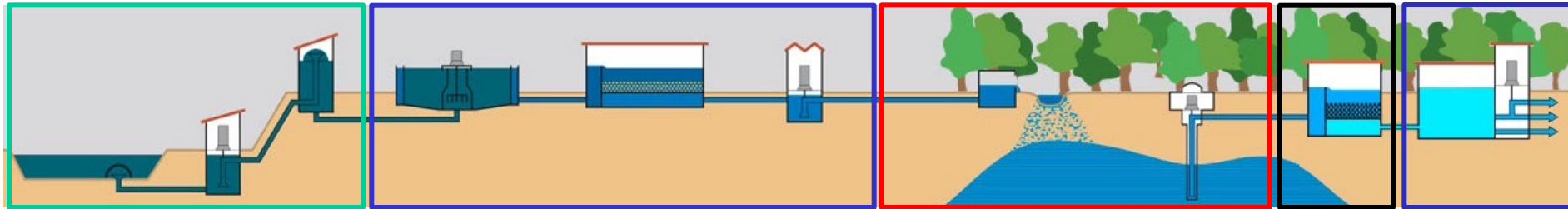
# Infiltration field Hardwald BL



8 m infiltration per day



# Artificial groundwater recharge: Hardwald, Baselland



**1. River Rhine  
pumping station**

**2. Pre-treatment**  
(Sedimentation / Rapid sand filtration)

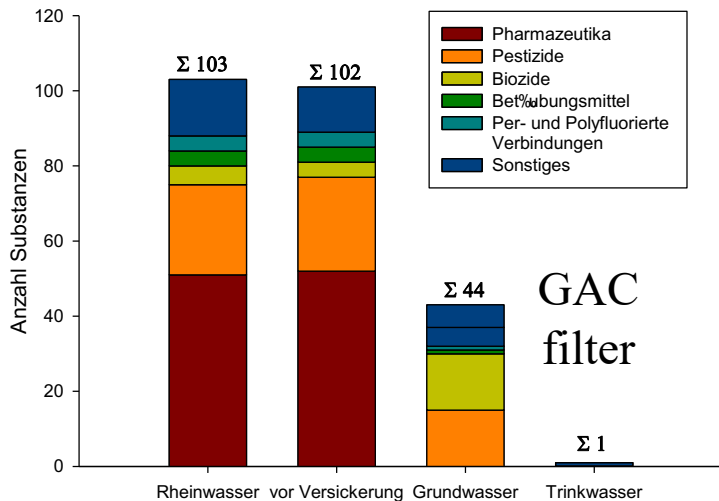
**3. Artificial recharge**  
(Hardwald forest)

**4. GAC  
filter**      **5. UV-  
Disinfection  
Distribution**

Particle removal

Biological  
treatment

Physical-  
chemical  
post-treatment

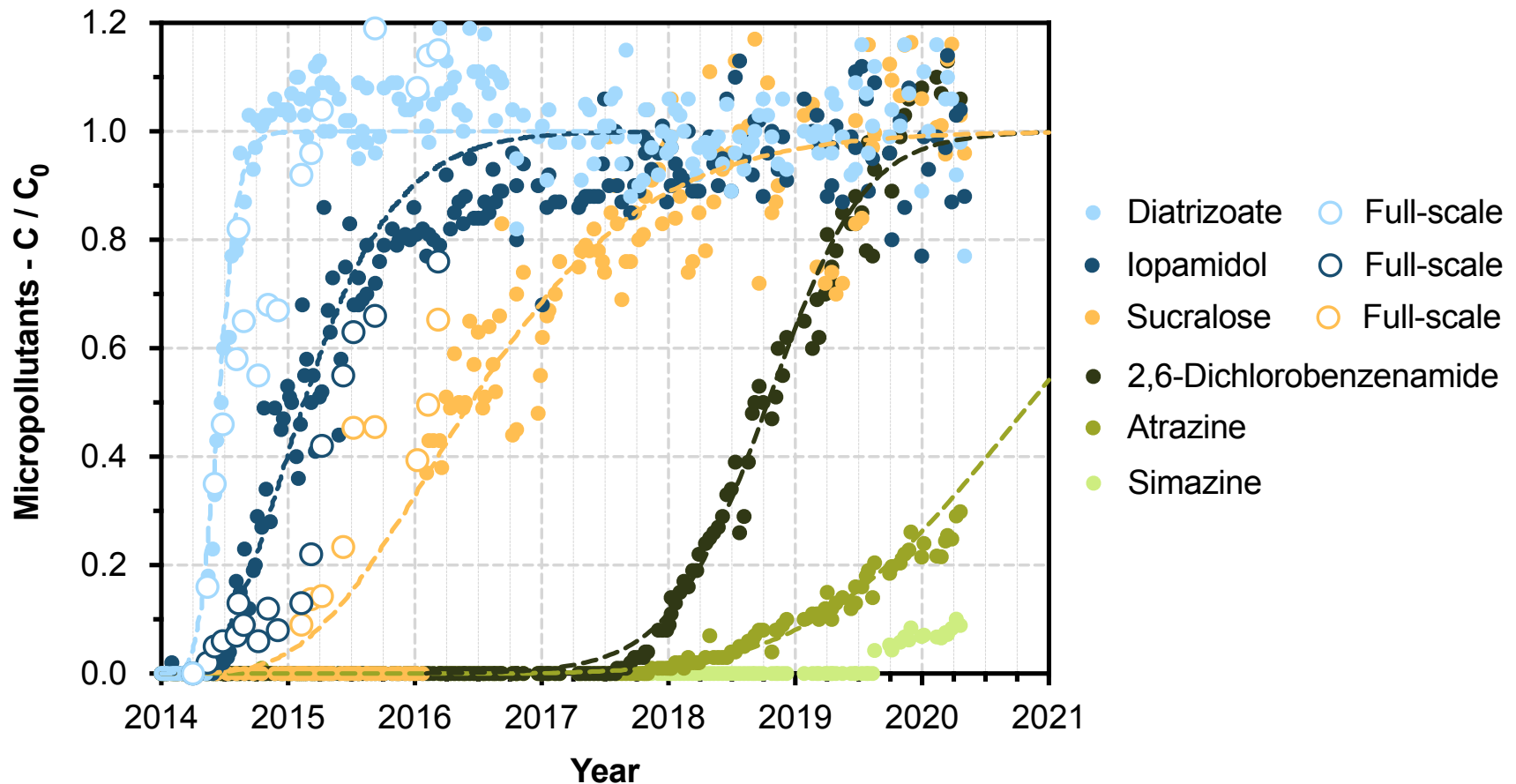


Rhine river  
Sandfilter  
Groundwater

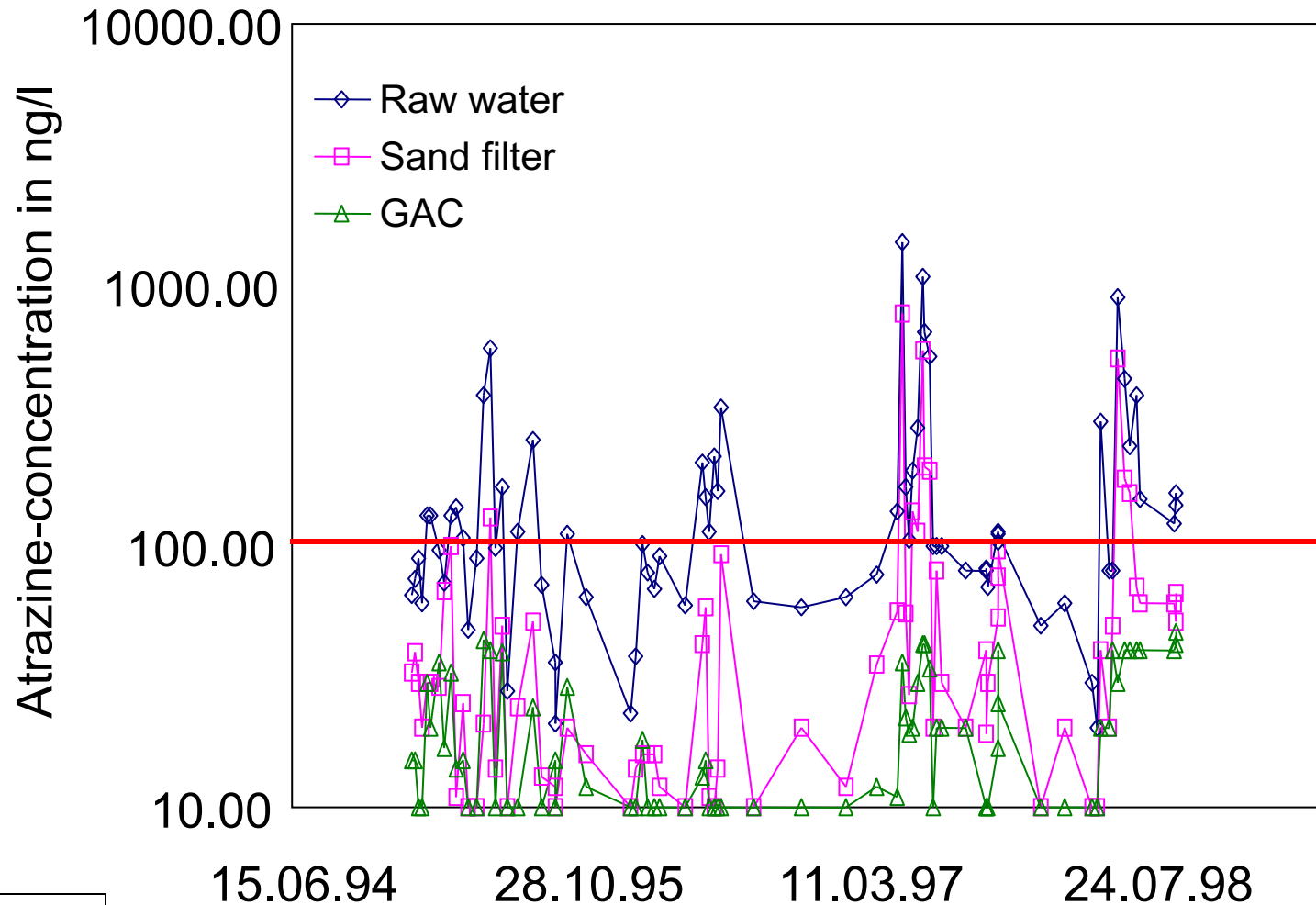
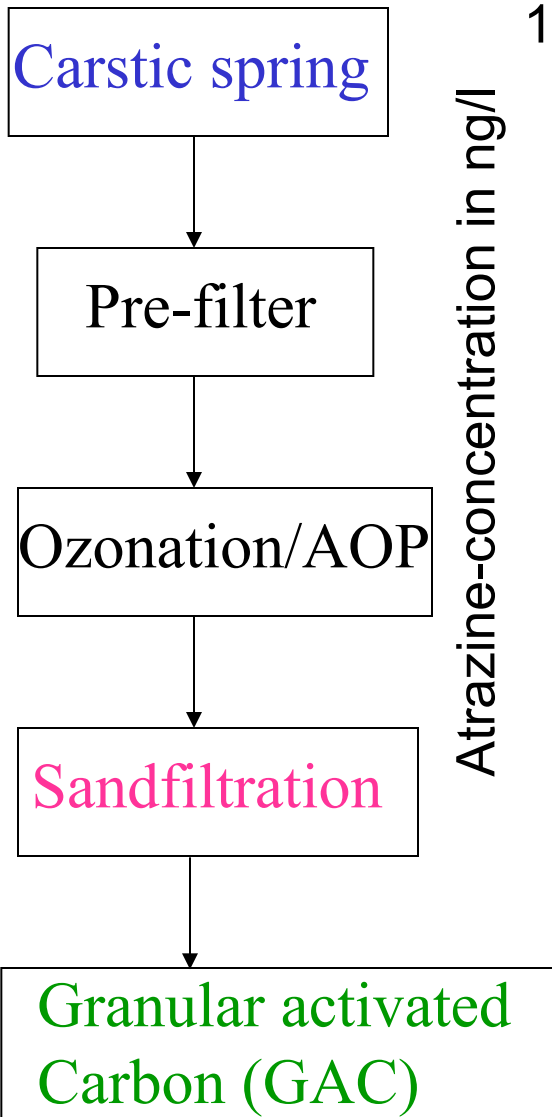
DOC 1.66 mg/L  
DOC 1.54 mg/L  
DOC 0.55 mg/L

# Activated carbon – Breakthrough of micropollutants (compared to iodinated contrast agents)

Rapid small-scale column tests and full-scale

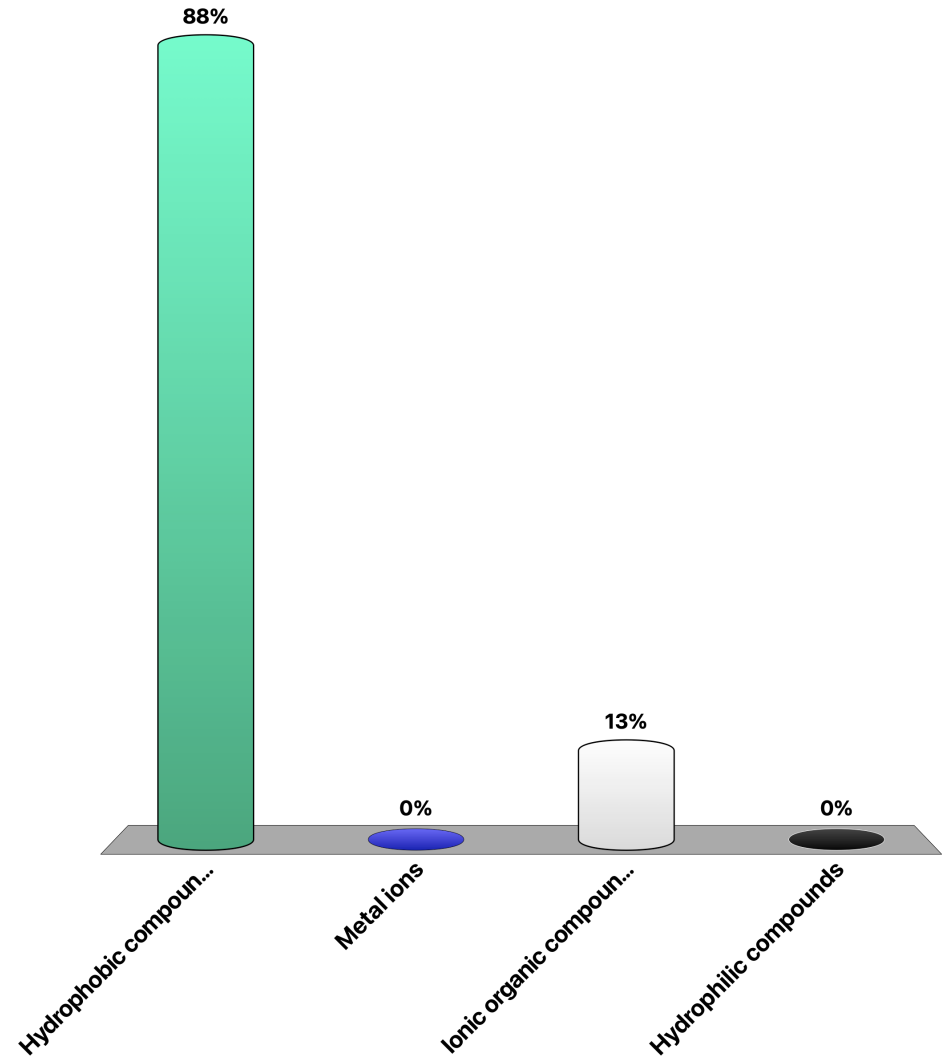


# Long-term behavior of the atrazine concentration in the water treatment plant Le Betteraz, Porrentruy JU

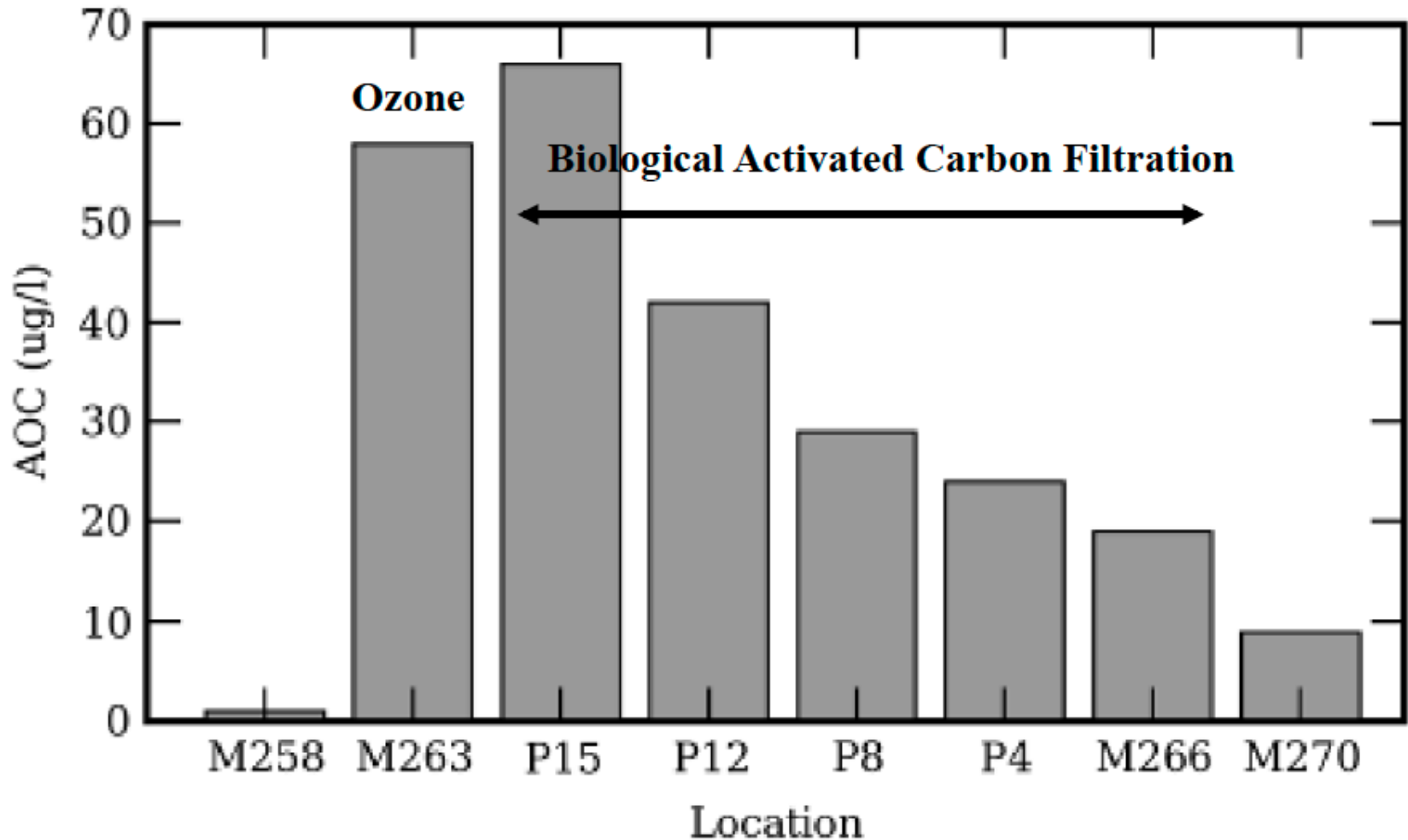


# Activated carbon is well suited for the removal of..

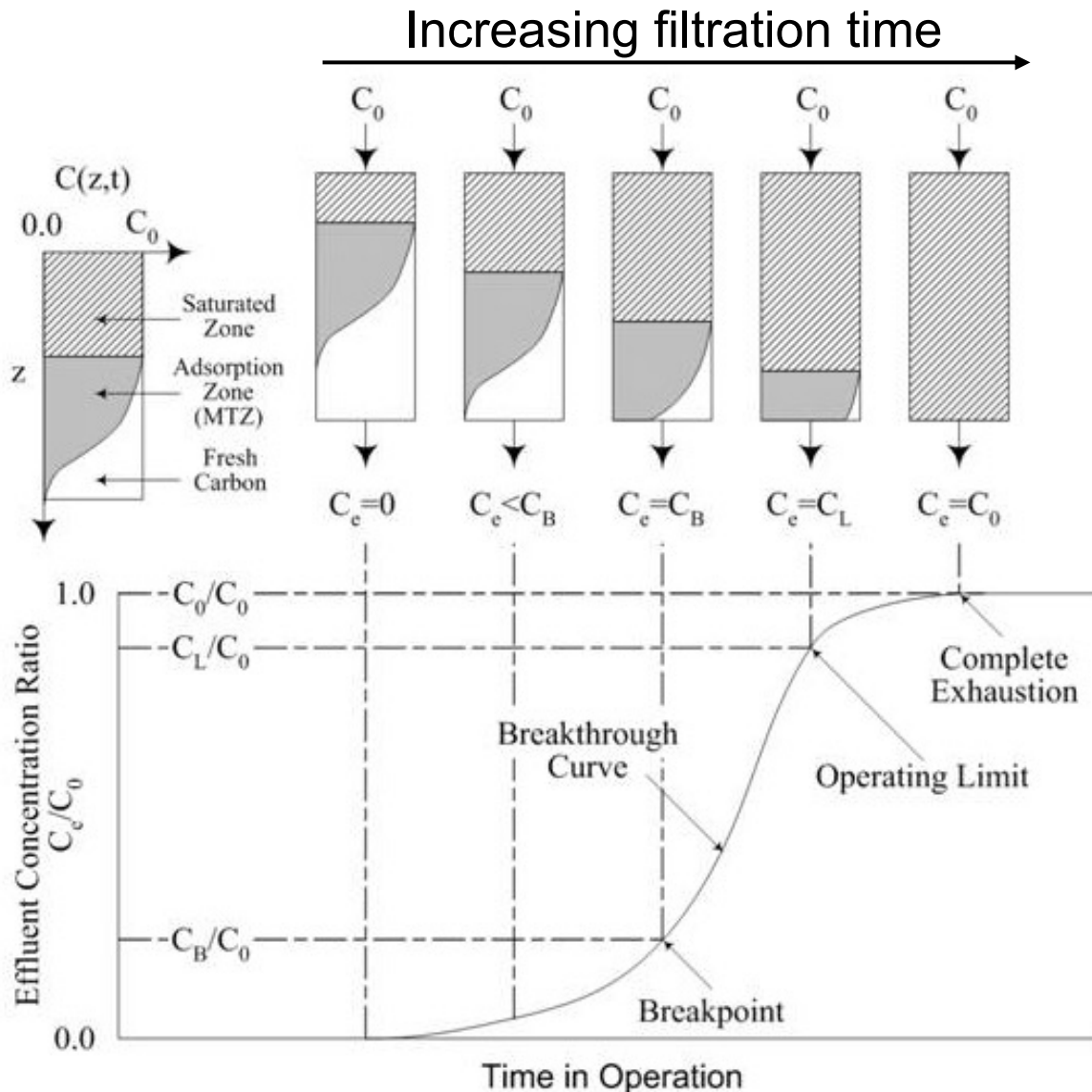
- A. Hydrophobic compounds
- B. Metal ions
- C. Ionic organic compounds
- D. Hydrophilic compounds



# Formation and elimination of assimilable organic carbon (AOC) during water treatment: Role of Biological Activated Carbon (BAC)



# Concentration profiles and breakthrough for GAC filters: Mass transfer zone (MTZ)



## Empty bed contact time (EBCT)

$$\text{EBCT} = \frac{V_F}{Q} = \frac{A_F L}{v A_F} = \frac{L}{v}$$

$V_F$ : volume occupied by adsorber media including porosity volume,  $\text{m}^3$

$Q$ : flow rate to adsorber,  $\text{m}^3/\text{h}$

$A_F$ : adsorber area available for flow,  $\text{m}^2$

$L$ : adsorber media depth,  $\text{m}$

$v$ : superficial flow velocity ( $Q/A_F$ ),  $\text{m}/\text{h}$

Range of EBCTs: 5-60 min for GAC

# Specific throughput and carbon usage rate

Specific throughput: volume fed to adsorber divided by mass of GAC m<sup>3</sup>/kg

$$\text{Specific throughput} = \frac{Qt_b}{M_{\text{GAC}}} = \frac{V_F t_b}{\text{EBCT} \times M_{\text{GAC}}} = \frac{V_F t_b}{\text{EBCT} \times \rho_F V_F} = \frac{t_b}{\text{EBCT} \times \rho_F}$$

L treated water / g GAC

$$Q = \frac{V_F}{\text{EBCT}}$$

$M_{\text{GAC}}$ : mass of GAC, kg

$t_b$ : time to breakthrough (treatment objective is exceeded)

$\rho_F$ : adsorber density or filter bed density, kg/m<sup>3</sup> ( $\rho_F = M_{\text{GAC}}/V_F$ )

## Carbon usage rate (CUR)

$$\text{CUR} = \frac{M_{\text{GAC}}}{Qt_b} = \frac{1}{\text{specific throughput}} \quad \text{g GAC / L treated water}$$



# Maximum specific throughput and carbon usage rate

When the adsorbate reaches the end of the filter, it is completely saturated.

This corresponds to the maximum specific throughput or the smallest carbon usage rate. All the adsorbate fed is adsorbed in the column and the adsorption capacity is in equilibrium with the influent concentration.

$$QC_{\text{inf}}t_b = M_{\text{GAC}}q_e(C_{\text{inf}})$$

$q_e(C_{\text{inf}})$  : adsorbent-phase concentration of the adsorbate at location  $z$  in equilibrium with the influent concentration, mg adsorbate/ mg adsorbent

$$\text{Maximum specific throughput} = \frac{Qt_b}{M_{\text{GAC}}} = \frac{q_e(C_{\text{inf}})}{C_{\text{inf}}}$$

$$\text{Minimum CUR} = \frac{M_{\text{GAC}}}{Qt_b} = \frac{C_{\text{inf}}}{q_e(C_{\text{inf}})}$$

# GAC running time

For an influent concentration  $C_{inf}$  and a target effluent concentration  $C_{eff}$ , the following equation can be formulated:

$$QC_{inf}t_b = Q \int_0^{t_b} C_{eff} dt + q_c M_{GAC}$$

$q_c$ : average adsorbent-phase concentration of adsorbate in GAC column, mg adsorbate/ g adsorbent

$C_{eff}$ : effluent liquid phase concentration at time  $t$ , mg/L

Specific throughput:

$$\frac{Qt_b}{M_{GAC}} = \frac{Q \int_0^{t_b} C_{eff} dt}{C_{inf} M_{GAC}} + \frac{q_c}{C_{inf}}$$

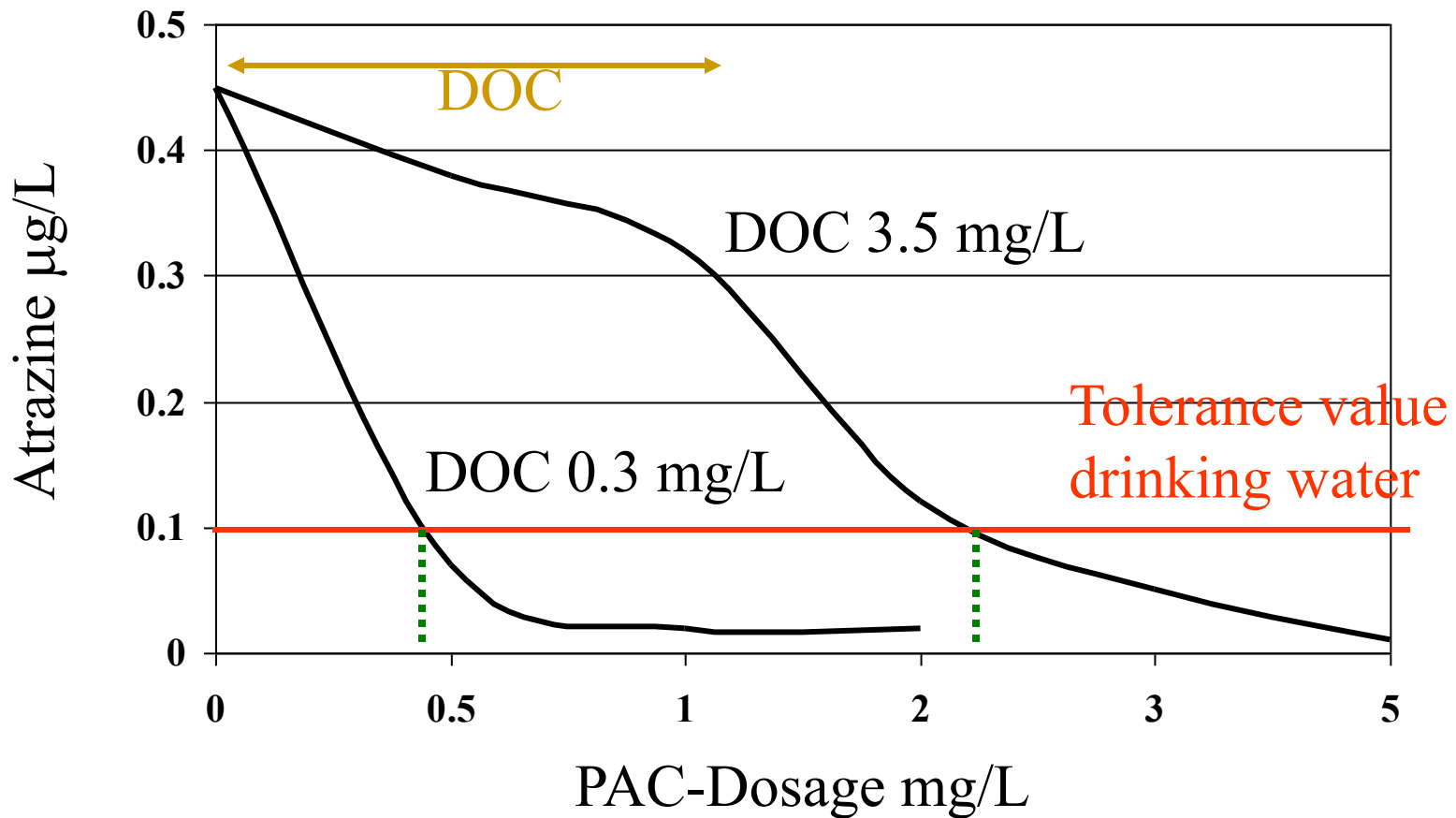
$$\text{if } C_{eff} \ll C_{inf} \Rightarrow \frac{Qt_b}{M_{GAC}} = \frac{q_c}{C_{inf}}$$

When the mass transfer zone is much smaller than the EBCT,  $q_c \approx q_e$

$$q_e = K \times (C_{inf})^{1/n}$$

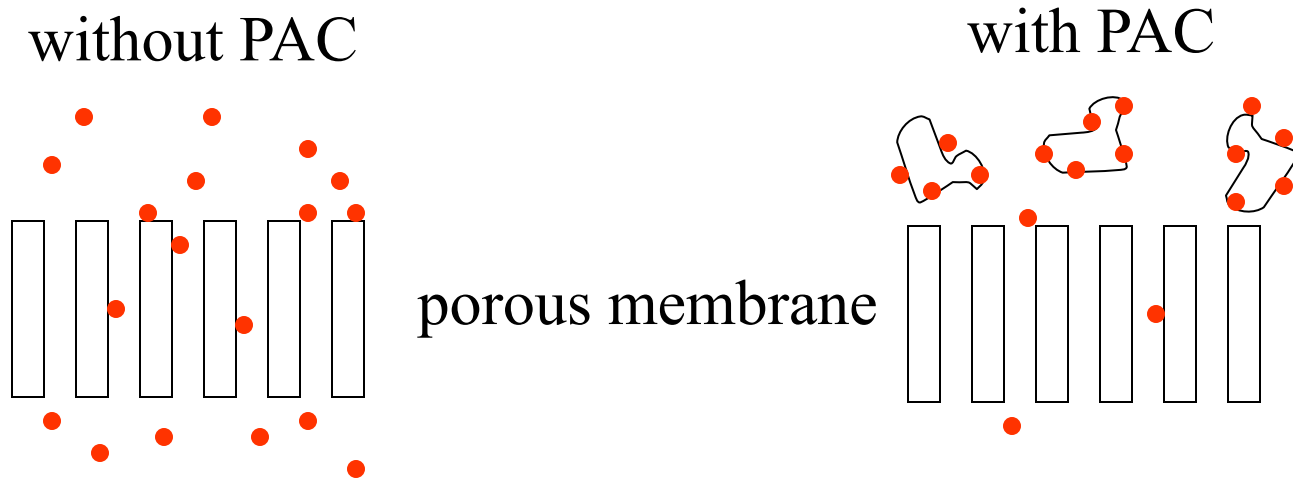
# Powdered activated carbon: influence of NOM

## Elimination of atrazine



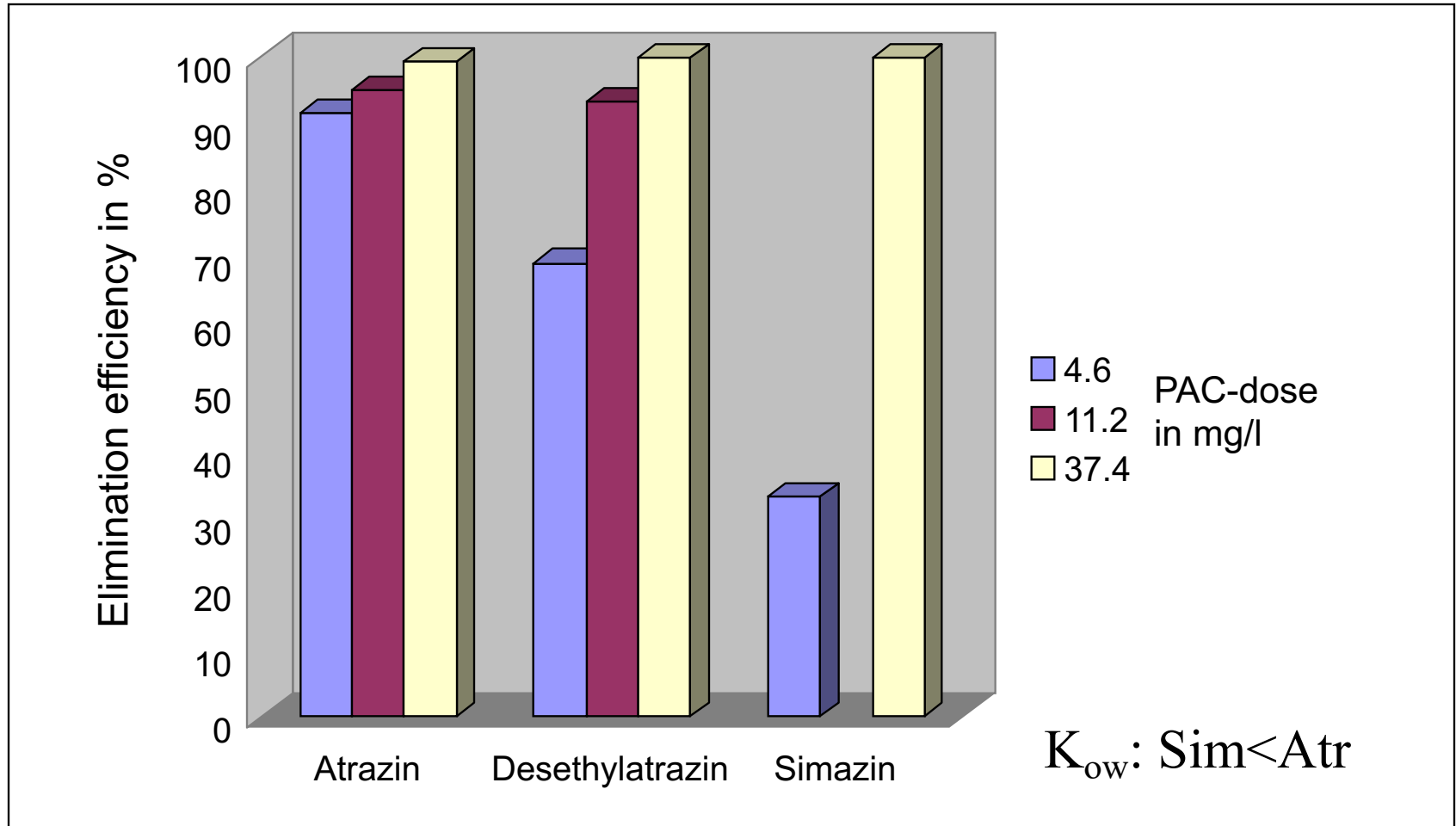
# Combination of PAC with membranes

- Adsorption of chemicals on particles
- larger pores in membranes (UF) → smaller pressure ( $\leq 5$  bar)



- Dosage on demand
- Simultaneous removal of NOM

# Elimination of pesticides by ultrafiltration combined with powdered activated carbon (PAC)

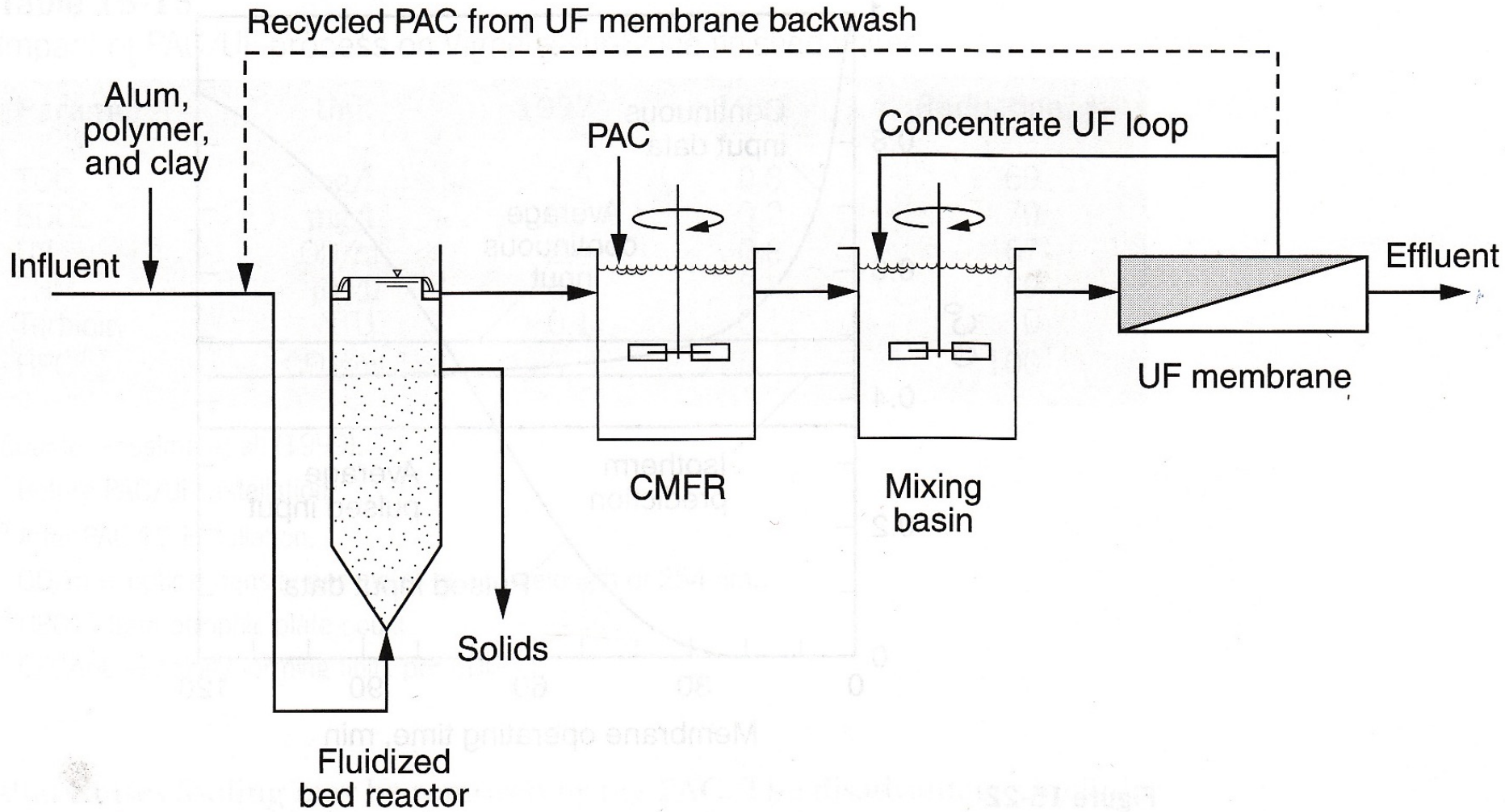


Ultrafiltration only → no elimination !

# PAC injection system, water supply Lausanne, Lutry



# PAC – Ultrafiltration (Vigneux sur Seine, F)



# Water quality parameters for PAC/UF process (Vigneux sur Seine)

<b>Parameter</b>	<b>Before PAC/UF installation</b>	<b>After PAC/UF installation</b>	<b>Reduction, %</b>
TOC mg/L	2.6	0.8	69
BDOC mg/L	0.7	0.2	70
Optical density 1/m	2.4	0.8	67
THM formation $\mu\text{g/L}$	73	8	89
Turbidity NTU	0.1	0.1	0
Colony forming units 1/mL	5	0	100



# Comparison GAC/PAC

<b>Parameter</b>	<b>Granular Activated Carbon (GAC)</b>	<b>Powdered Activated Carbon (PAC)</b>
Main uses	<ul style="list-style-type: none"><li>• Control of toxic organic compounds in groundwaters</li><li>• Barrier against micropollutants in surface waters (e.g. taste and odor)</li><li>• Control of DOC</li></ul>	<ul style="list-style-type: none"><li>• Seasonal control of micropollutants (e.g. taste and odor, pesticides)</li></ul>
Advantages	<ul style="list-style-type: none"><li>• Can be regenerated</li><li>• Lower carbon usage rate per volume of water treated compared to PAC</li></ul>	<ul style="list-style-type: none"><li>• Easily added to existing coagulation for occasional control of organics</li></ul>
Disadvantages	<ul style="list-style-type: none"><li>• Need contactors and infrastructure for regeneration</li><li>• Previously adsorbed compounds can desorb</li></ul>	<ul style="list-style-type: none"><li>• Hard to regenerate and recover from sludge</li><li>• Higher carbon usage rate per volume water treated compared to GAC</li></ul>

# Conclusions

- Two forms of AC application: granular activated carbon filters and powdered activated carbon
- Activated carbon can be used as a polishing treatment to remove micropollutants; mostly integrated into multi-step treatment
- Adsorption of micropollutants can be described by empirical adsorption laws, affinity depends on hydrophobic character
- DOM competes with adsorbates and reduces the adsorption capacity
- GAC is often used as biological filtration step: BAC